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EV	AMINER INTERVIEW SUMMARY RECORD	TE MAILED:	
EX	AMINER INTERVIEW SOMMART RECORD	,	
II participants (applicant, applicant's representativ			, _)
1) Eric W. Guttag/Geor	yow. Allen (3) Everett	White (PTOJ
2) Pat J. Corriga	you. Allum (3) Everett (4) Johnnie K	2. Brown	<u> </u>
Date of interview May 28, 1992			
ype: Telephonic Personal (copy is given	n to applicant applicant's representative).		
xhibit shown or demonstration conducted: 🚨 Y	es		
dentification of prior art discussed: $\frac{\alpha}{-}$	ic prior art of record.		
	d to if an agreement was reached, or any other comme	The Ather	and property to selling
chim 62, that's attach, which	more clearly define the invention	n. It is the	e txaminer's opinion
hot this new claim will require	e further consideration and fourth	her seapch.	Mr. Corrigan expl
he mechanism of the invent	ion. Attorney Guttag question	ed why US	Patent No 5,043,43
nd European Patent No. 383,404	were not applied against the	dains. T	his may have been
yer sight in the part of the Education of the fuller description, if necessary, and a copy of the amendments with the second sec	the amendments, if available, which the examiner agr which would render the claims allowable is available, a	eed would render summary thereof n	the claims allowable must be nust be attached.)
OT WAIVED AND MUST INCLUDE THE SUBS	indicate to the contrary, A FORMAL WRITTEN RISTANCE OF THE INTERVIEW (e.g., items $1-7$ on the ant is given one month from this interview date to pro-	he reverse side of t	his form). If a response to the
It is not necessary for applicant to provide a	separate record of the substance of the interview.		
	ove (including any attachments) reflects a complete ro t Office action, and since the claims are now allowable on.		
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PROPOSED NEW CLAIM 62 FOR CASE 4233

- 62. A continuous process for preparing highly esterified polyol fatty acid polyester by interesterifying polyol containing more than about four esterifiable hydroxy groups and fatty acid ester of easily removable alcohol in a heterogeneous reaction mixture wherein said easily removable alcohol is removed, said process comprising an improvement selected from the group consisting of:
 - the initial stage of the reaction is carried out in a continuous manner under conditions of backmixing to maintain a level of lower partial fatty acid esters of said polyol in an emulsifying amount;
 - (2) at least the final stage of the reaction is carried out in a continuous manner under conditions approaching plug-flow conditions after the degree of esterification of said polyol is at least about 50%; and
 - (3) a combination of improvements (1) and (2).

Support for new Claim 62: Claim 1, Claim 34 and page 23, lines 19-21.

(4233R3)

Interview for Case 4233

- I. Applicants' Claimed Improved, Preferably Continuous, Processes for Preparing Highly Esterified Polyol Polyesters
 - A. Ten separate process improvements, plus combinations of these improvements. See Claim 1.
 - B. Claimed process improvements offer a number of significant advantages, including:
 - 1. increased reaction speed and efficiency;
 - 2. reduced/minimized formation of undesired/unwanted by-products;
 - 3. reduced/minimized need to remove excess reactants/catalyst
 - greater conversion to desired highly esterified polyol polyester end products
 - 5. easier clean-up of desired end products
 - 6. reduced/minimized capacity/energy requirements for equipment used and increased process flexibility.
 - C. Handout Explaining Reaction Chemistry of Claimed Process
 Improvements (Pat Corrigan)

- 1. In general.
- 2. As it relates specifically to "backmixing" in initial stage and "plug-flow" in final stage(s).

II. Proposed New Claim 62

- A. Recites continuous process involving:
 - "backmixing" conditions in initial stage to maintain emulsifying amount of partial esters;
 - "plug-flow" conditions in final stage(s) after degree of esterification reaches 50%; and
 - 3. combination of "back mixing" and "plug-flow" conditions.
- B. If allowable, Claims 14-16, 27-51 and 54-58 would be amended to depend therefrom.

III. The Rejection of Claims 1, 14-16, 27-51 and 54-58 under 35 USC 103 over Volpenhein, in View of Osipow et al, as it Relates to "Backmixing" and "Plug-Flow."

A. "Backmixing"

- Requires: (a) continual recycling of portion of reactant mixture; or (b) carrying out reaction in agitated vessel(s) with continual addition of reactants and removal of product.
 See paragraph bridging pages 19-20 of Case 4233.
- Volpenhein and Osipow et al nowhere teach reaction conditions that inherently involve "backmixing."

B. "Plug-FLow"

- Requires (a) feeding output of initial stage into at least 2 CSTRs; or (b) use of continuous reactor, e.g., tubular reactor.
 See page 21, lines 27-33 of Case 4233.
- Volpenhein and Osipow et al nowhere teach reaction conditions that inherently involve "plug-flow."

Sucrose Polyester

Reaction Chemistry

The sucrose polyester reaction has four main raw materials:

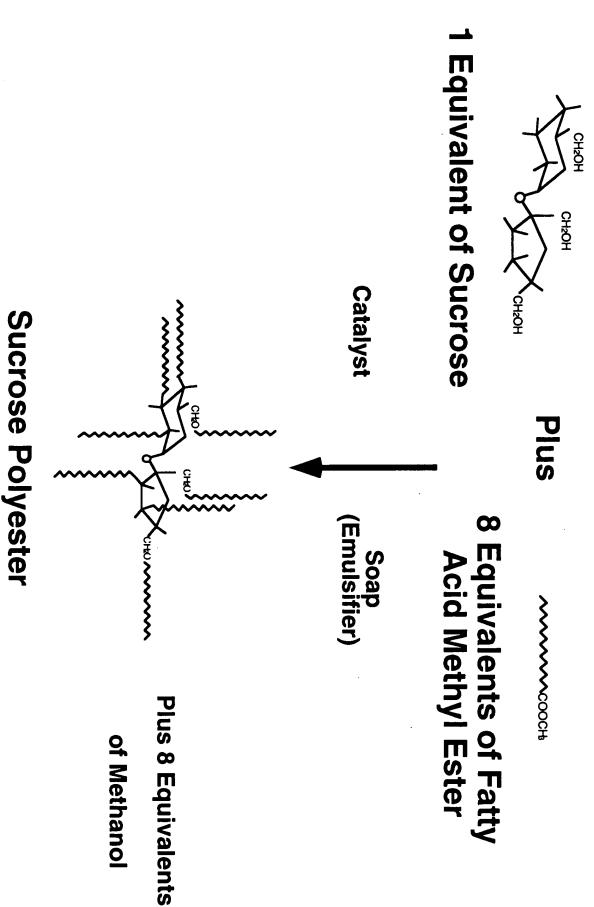
Sucrose

Fatty Acid Methyl Esters

Soap

Catalyst

Basic Sucrose Polyester Reaction



Sucrose Polyester Reaction Involves 2 Steps:

Solubilize the solid sucrose into the liquid methyl esters

2. Esterify the methyl esters with the sucrose

Materials that help solubilize the sucrose:

~~~~C00-K+

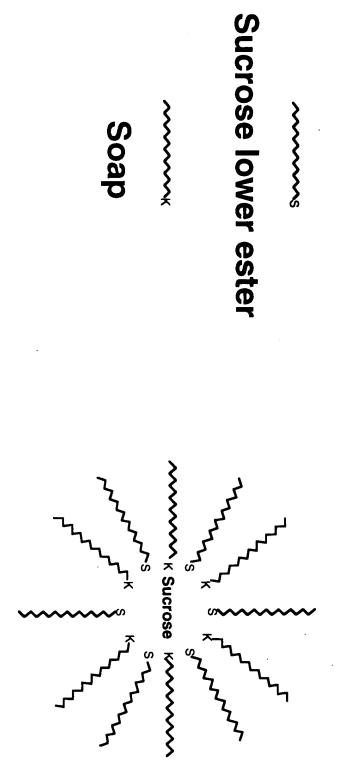
(Soap)

CH2OH CH2OH

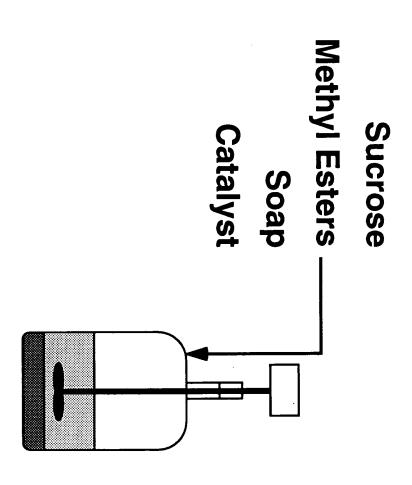
**Lower Esters of Sucrose** 

**Both** are required

## **Inverted Micelles**



## **Batch Reaction**

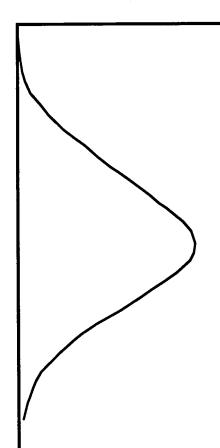


First part of the reaction:

Sucrose + Methyl Ester -----> Sucrose Lower Esters

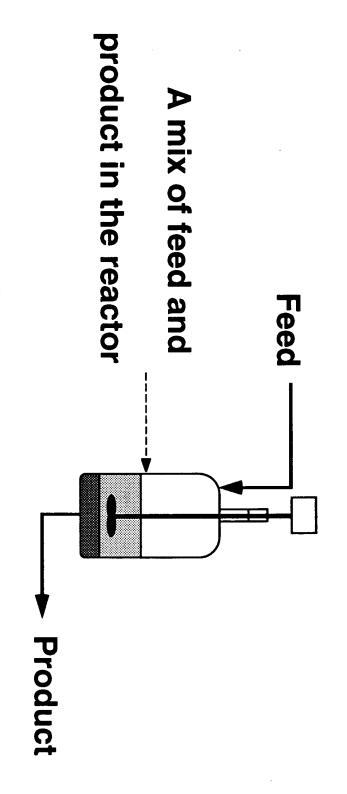
# **Sucrose Lower Esters versus Time**

Amount of Sucrose
Lower Esters



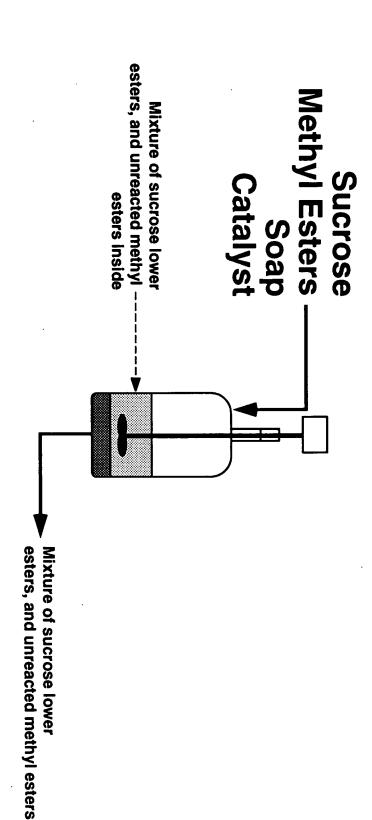
Reaction Time ---->

# **A Continuous Backmixed Reactor**



# A Continuous Backmixed Reactor

## to Make Sucrose Lower Esters



the basic reaction for the formation of sucrose polyester Once the sucrose has reacted to sucrose lower ester, S

sucrose ester + methyl ester sucrose polyester + methanol

Reaction rate = 
$$\Re = \frac{k[SE_i][ME]}{[MeOH]}$$

There is an excess of methyl esters in the reaction: [ME] -----> constant (with respect to [SE<sub>i</sub>])

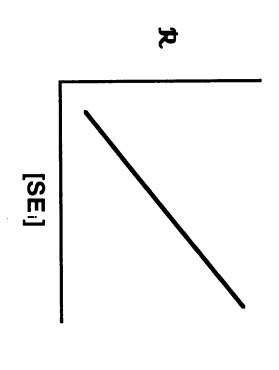
[MeOH] ----> also constant with respect to [SE<sub>i</sub>]. Methanol is continuously removed by vacuum:

Then: 2 = K[SEi]

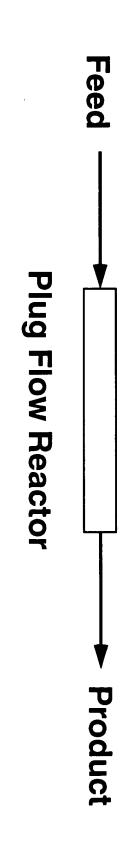
where K = k[ME]
[MeOH]

R is proportional to [SE<sub>i</sub>]

ℜ is proportional to [SE<sub>i</sub>]



## Plug Flow Reactor

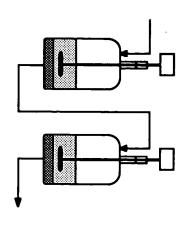


a plug flow reactor

is equivalent to

2 or more back-

mixed reactors



## **Final Conclusions:**

The optimum method to run this reaction on a practical scale is:

1. Run the first part of the reaction in a continuous, backmixed mode;

2. Run the subsequent part of the reaction in a plug flow mode.